# 04-CHEM-B1, TRANSPORT PHENOMENA

# May 2016

## 3 hours duration

### **NOTES**

- 1. If doubt exists as to the interpretation of any question, the candidate is urged to submit with the answer paper, a clear statement of any assumptions made.
- 2. The examination is an **open book exam.** One textbook of your choice with notations listed on the margins etc., but no loose notes are permitted into the exam.
- 3. Candidates may use any **non-communicating** calculator.
- 4. All problems are worth 25 points. **One problem** from **each** of sections A, B, and C must be attempted. A **fourth** problem from **any section** must also be attempted.
- 5. Only the first four questions as they appear in the answer book will be marked.
- 6. State all assumptions clearly.

May 2016

#### Section A: Fluid Mechanics

- A1. The simplest patient infusion system is that of gravity flow from an intravenous (IV) bag. A 500 ml IV bag containing an aqueous solution is connected to a vein in the forearm of a patient. Venous pressure in the forearm is 0 mm Hg (gage pressure). The IV bag is placed on a stand such that the entrance to the tube leaving the IV bag is exactly 1 meter above the vein into which the IV fluid enters. The length of the IV bag is 30 cm. The IV is fed through an 18-gage tube (internal diameter = 0.953 mm) and the total length of the tube is 2 meters. Calculate the flow rate of the IV fluid, and estimate the time needed to empty the IV bag.
- A2. The spin coating process is used to coat a thin film of photoresist (organic polymer) on the wafer. A viscous solution containing the photoresist material is made to form a thin (~ 1  $\mu$ m) uniform thin film on the wafer by spinning the wafer as shown in the figure below.



- a) [22 points] Derive an expression for thickness of the film on the wafer (h) as a function time (t), angular velocity ( $\omega$ ), and the kinematic viscosity ( $\nu$ ) of the photoresist solution.
- b) [3 points] What is the corresponding equation for thickness of a very thin film of photoresist on the wafer?

# 04-CHEM-B1, Transport Phenomena May 2016

### Section B: Heat Transfer

**B1.** Air at 1 atm and 150 °C enters a pipe of diameter 5.08 cm, and it is heated as it moves through the pipe at a velocity of 8 m/s. Assume constant heat flux per unit length of the pipe, and that the pipe wall temperature is 20 °C above air temperature.

a) [18 points] Determine the heat transfer per unit length of the pipe.

b) [7 points] Calculate the bulk temperature rise through a 2-meter length of pipe.

### DATA:

Thermal conductivity of air =  $3.52 \times 10^{-2}$  W/m °C Viscosity of air =  $2.38 \times 10^{-5}$  kg/m.s Specific heat capacity of air = 1.017 kJ/kg °C Molecular weight of air = 29 g/mol

**B2.** Derive the differential energy balance equation in spherical coordinates for heating a sphere of radius r, if the temperature variation with angular position is zero.

#### Section C: Mass Transfer

**C1.** For rate of mass transfer from a cylinder rotating in a liquid bath, the Sherwood number (Sh) is given by the equation

$$Sh = k_d / U_r = 0.079 (Re)^{-0.3} (Sc)^{-0.644}$$

where  $k_d$  is the mass transfer coefficient between cylinder and liquid,  $U_r$  is the peripheral speed of rotation, Schmidt number (Sc) = v/D<sub>AB</sub>, Reynold's number (Re) = dU/v, and kinematic viscosity (v) =  $\mu/\rho$ .

In an experiment, a 1.5-cm diameter by 5.0-cm long iron cylinder was rotated at a speed of 77 rpm in a melt of carbon-saturated iron at 1275 °C. The rate of dissolution, expressed as decrease of rod radius with time, was  $-5.57 \times 10^{-3}$  cm/s. For the dissolution of iron in carbon-saturated iron, the iron mass concentration driving force ( $\Delta X_{Fe}$ ) was estimated to be 0.385. Assuming the densities of the iron rod and the carbon-saturated iron melt are equal, compare the experimental rate of dissolution with that predicted by the above correlation.

#### DATA:

Diffusivity of iron in the carbon-saturated iron melt at 1275  $^{\circ}C = 9 \times 10^{-5} \text{ cm}^2/\text{s}$ Kinematic viscosity of iron melt at 1275  $^{\circ}C = 1.41 \times 10^{-2} \text{ cm}^2/\text{s}$ 

- **C2.** During class break, a guy comes and cleans the blackboards. He leaves a thin film of water whose thickness is 1 mm. Water evaporates from that surface into the surrounding air, whose humidity is 10%. We want to calculate how long it takes for the water to evaporate completely. Assume a diffusional distance between the water surface and ambient air of 1 cm. At 25 °C, the vapor pressure of water is 0.0313 atm, and the diffusion coefficient of water vapor in air is 0.282 cm<sup>2</sup>/s.
  - a) [3 points] Define the problem, draw coordinates, and state assumptions.
  - b) [13 points] Calculate the steady-state flux of water from the surface.
  - c) [2 points] Obtain an expression to relate the flux to the disappearance of liquid water.
  - d) [7 points] Calculate the time required for the water film to evaporate and the chalkboard to dry completely.

#### 04-CHEM-B1, Transport Phenomena

May 2016

#### **APPENDIX A**

## **Summary of the Conservation Equations**

#### **Table A.1 The Continuity Equation**

$$\frac{\partial \rho}{\partial t} + \left(\nabla \cdot \rho \vec{u}\right) = 0 \tag{1.1}$$

Rectangular coordinates (x, y, z)

$$\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x} (\rho u_x) + \frac{\partial}{\partial y} (\rho u_y) + \frac{\partial}{\partial z} (\rho u_z) = 0$$
(1.1a)

Cylindrical coordinates  $(r, \theta, z)$ 

$$\frac{\partial \rho}{\partial t} + \frac{1}{r} \frac{\partial}{\partial r} (\rho r u_r) + \frac{1}{r} \frac{\partial}{\partial \theta} (\rho u_\theta) + \frac{\partial}{\partial z} (\rho u_z) = 0$$
(1.1b)

Spherical coordinates 
$$(r, \theta, \phi)$$
  

$$\frac{\partial \rho}{\partial t} + \frac{1}{r^2} \frac{\partial}{\partial r} (\rho r^2 u_r) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (\rho u_\theta \sin \theta) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \phi} (\rho u_\phi) = 0 \qquad (1.1c)$$

#### Table A.2 The Navier-Stokes equations for Newtonian fluids of constant $\rho$ and $\mu$

$$\frac{\partial \vec{u}}{\partial t} + (\vec{u} \cdot \nabla) \overline{u} = -\frac{1}{\rho} \nabla P + \vec{g} + \nu \left( \nabla^2 \vec{u} \right)$$
(A2)

**Rectangular coordinates** (x, y, z) x-component  $\frac{\partial u_x}{\partial t} + u_x \frac{\partial u_x}{\partial x} + u_y \frac{\partial u_x}{\partial y} + u_z \frac{\partial u_x}{\partial z} = -\frac{1}{\rho} \frac{\partial P}{\partial x} + g_x + v \left( \frac{\partial^2 u_x}{\partial x^2} + \frac{\partial^2 u_x}{\partial y^2} + \frac{\partial^2 u_x}{\partial z^2} \right)$  (A2a)  $\frac{\partial u_y}{\partial x} + \frac{\partial u_y}{\partial x} + \frac{\partial u_y}{\partial y} + \frac{\partial u_y}{\partial x} + \frac{1}{\rho} \frac{\partial P}{\partial x} + g_z + v \left( \frac{\partial^2 u_y}{\partial x^2} + \frac{\partial^2 u_y}{\partial y^2} + \frac{\partial^2 u_y}{\partial z^2} \right)$  (A2b)

*y*-component 
$$\frac{\partial u_y}{\partial t} + u_x \frac{\partial u_y}{\partial x} + u_y \frac{\partial u_y}{\partial y} + u_z \frac{\partial u_y}{\partial z} = -\frac{1}{\rho} \frac{\partial P}{\partial y} + g_y + \nu \left( \frac{\partial u_y}{\partial x^2} + \frac{\partial u_y}{\partial y^2} + \frac{\partial u_y}{\partial z^2} \right)$$
(A2b)

*z*-component 
$$\frac{\partial u_z}{\partial t} + u_x \frac{\partial u_z}{\partial x} + u_y \frac{\partial u_z}{\partial y} + u_z \frac{\partial u_z}{\partial z} = -\frac{1}{\rho} \frac{\partial P}{\partial z} + g_z + v \left( \frac{\partial^2 u_z}{\partial x^2} + \frac{\partial^2 u_z}{\partial y^2} + \frac{\partial^2 u_z}{\partial z^2} \right)$$
 (A2c)

### 04-CHEM-B1, Transport Phenomena May 2016

Cylindrical coordinates  $(r, \theta, z)$  $\frac{\partial u_r}{\partial t} + u_r \frac{\partial u_r}{\partial t} + \frac{u_{\theta}}{u} \frac{\partial u_r}{\partial t} + u_z \frac{\partial u_r}{\partial t} - \frac{u_{\theta}^2}{u}$ *r*-component  $= -\frac{1}{2}\frac{\partial P}{\partial r} + g_r + v \left[ \frac{\partial}{\partial r} \left( \frac{1}{r} \frac{\partial (ru_r)}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 u_r}{\partial \theta^2} - \frac{2}{r^2} \frac{\partial u_{\theta}}{\partial \theta} + \frac{\partial^2 u_r}{\partial r^2} \right]$ (A2d)  $\frac{\partial u_{\theta}}{\partial t} + u_r \frac{\partial u_{\theta}}{\partial t} + \frac{u_{\theta}}{r} \frac{\partial u_{\theta}}{\partial \theta} + u_z \frac{\partial u_{\theta}}{\partial t} + \frac{u_r u_{\theta}}{r}$  $= -\frac{1}{2r}\frac{\partial P}{\partial \theta} + g_{\theta} + v \left[\frac{\partial}{\partial r}\left(\frac{1}{r}\frac{\partial(ru_{\theta})}{\partial r}\right) + \frac{1}{r^{2}}\frac{\partial^{2}u_{\theta}}{\partial \theta^{2}} + \frac{2}{r^{2}}\frac{\partial u_{r}}{\partial \theta} + \frac{\partial^{2}u_{\theta}}{\partial r^{2}}\right]$  $\theta$ -component (A2e) $\frac{\partial u_z}{\partial t} + u_r \frac{\partial u_z}{\partial t} + \frac{u_\theta}{u_r} \frac{\partial u_z}{\partial t} + u_z \frac{\partial u_z}{\partial t}$ z-component  $= -\frac{1}{2}\frac{\partial P}{\partial r} + g_z + v \left| \frac{1}{r}\frac{\partial}{\partial r} \left( r\frac{\partial u_z}{\partial r} \right) + \frac{1}{r^2}\frac{\partial^2 u_z}{\partial \theta^2} + \frac{\partial^2 u_z}{\partial z^2} \right|$ (A2f)Spherical coordinates  $(r, \theta, \phi)$  $\frac{\partial u_r}{\partial t} + u_r \frac{\partial u_r}{\partial r} + \frac{u_{\theta}}{r} \frac{\partial u_r}{\partial \theta} + \left(\frac{u_{\phi}}{r \sin \theta}\right) \frac{\partial u_r}{\partial \phi} - \frac{u_{\theta}^2}{r} - \frac{u_{\phi}^2}{r} = -\frac{1}{\rho} \frac{\partial P}{\partial r} + g_r$ (A2g)*r*-component  $+ \nu \left[ \frac{1}{r^2} \frac{\partial^2}{\partial r^2} (r^2 u_r) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} (\sin \theta \frac{\partial u_r}{\partial \theta}) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 u_r}{\partial \theta^2} \right]$  $\frac{\partial u_{\theta}}{\partial t} + u_r \frac{\partial u_{\theta}}{\partial r} + \frac{u_{\theta}}{r} \frac{\partial u_{\theta}}{\partial \theta} + \left(\frac{u_{\phi}}{r\sin\theta}\right) \frac{\partial u_{\theta}}{\partial \phi} + \frac{u_r u_{\theta}}{r} - \frac{u_{\phi}^2}{r} \cot\theta = -\frac{1}{\rho r} \frac{\partial P}{\partial \theta} + g_{\theta}$  $+ v \left| \frac{\frac{1}{r^2} \frac{\partial}{\partial r} \left( r^2 \frac{\partial u_{\theta}}{\partial r} \right) + \frac{1}{r^2} \frac{\partial}{\partial \theta} \left( \frac{1}{\sin \theta} \frac{\partial}{\partial \theta} \left( u_{\theta} \sin \theta \right) \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 u_{\theta}}{\partial \phi^2} \right| \\ + \frac{2}{r^2} \frac{\partial u_r}{\partial \theta} - \frac{2 \cot \theta}{r^2 \sin \theta} \frac{\partial u_{\phi}}{\partial \phi}$  $\theta$ -component (A2h)  $\frac{\partial u_{\phi}}{\partial t} + u_r \frac{\partial u_{\phi}}{\partial r} + \frac{u_{\theta}}{r} \frac{\partial u_{\phi}}{\partial \theta} + \frac{u_{\phi}}{r \sin \theta} \frac{\partial u_{\phi}}{\partial \phi} + \frac{u_r u_{\phi}}{r} + \frac{u_{\theta} u_{\phi}}{r} \cot \theta = -\frac{1}{\rho r \sin \theta} \frac{\partial P}{\partial \phi}$  $+g_{\varphi}+\nu \left| \begin{array}{c} \frac{1}{r^{2}}\frac{\partial}{\partial r}\left(r^{2}\frac{\partial u_{\phi}}{\partial r}\right)+\frac{1}{r^{2}}\frac{\partial}{\partial \theta}\left(\frac{1}{\sin\theta}\frac{\partial}{\partial\theta}\left(u_{\phi}\sin\theta\right)\right)+\frac{1}{r^{2}\sin^{2}\theta}\frac{\partial^{2}u_{\phi}}{\partial\phi^{2}}\right| \\ +\frac{2}{r^{2}\sin\theta}\frac{\partial u_{r}}{\partial\phi}+\frac{2\cot\theta}{r^{2}\sin\theta}\frac{\partial u_{\theta}}{\partial\phi} \end{array} \right|$  $\phi$ -component (A2i)

## 04-CHEM-B1, Transport Phenomena May 2016

## Table A.3 The Energy Equation for Incompressible Media

$$\rho c_{P} \left[ \frac{\partial T}{\partial t} + (\vec{u} \cdot \nabla)(T) \right] = \left[ \nabla \cdot k \nabla T \right] + \dot{T}_{G}$$
(A3)

Rectangular coordinates (x, y, z)

$$\rho c_{P} \left[ \frac{\partial T}{\partial t} + u_{x} \frac{\partial T}{\partial x} + u_{y} \frac{\partial T}{\partial y} + u_{z} \frac{\partial T}{\partial z} \right] = \frac{\partial}{\partial x} \left( k \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left( k \frac{\partial T}{\partial y} \right) + \frac{\partial}{\partial z} \left( k \frac{\partial T}{\partial z} \right) + \dot{T}_{G}$$
(A3a)

Cylindrical coordinates  $(r, \theta, z)$ 

$$\rho c_{P} \left[ \frac{\partial T}{\partial t} + u_{r} \frac{\partial T}{\partial r} + \frac{u_{\theta}}{r} \frac{\partial T}{\partial \theta} + u_{z} \frac{\partial T}{\partial z} \right] = \frac{1}{r} \frac{\partial}{\partial r} \left( rk \frac{\partial T}{\partial r} \right) + \frac{1}{r^{2}} \frac{\partial}{\partial \theta} \left( k \frac{\partial T}{\partial \theta} \right) + \frac{\partial}{\partial z} \left( k \frac{\partial T}{\partial z} \right) + \dot{T}_{G}$$
(A3b)

Spherical coordinates 
$$(r, \theta, \phi)$$

$$\rho c_{p} \left[ \frac{\partial T}{\partial t} + u_{r} \frac{\partial T}{\partial r} + \frac{u_{\theta}}{r} \frac{\partial T}{\partial \theta} + \frac{u_{\phi}}{r \sin \theta} \frac{\partial T}{\partial \phi} \right] = \frac{1}{r^{2}} \frac{\partial}{\partial r} \left( r^{2} k \frac{\partial T}{\partial r} \right) + \frac{1}{r^{2} \sin \theta} \frac{\partial}{\partial \theta} \left( k \sin \theta \frac{\partial T}{\partial \theta} \right) + \frac{1}{r^{2} \sin^{2} \theta} \frac{\partial}{\partial \phi} \left( k \frac{\partial T}{\partial \phi} \right) + \dot{T}_{G}$$
(A3c)

## Table A4: The continuity equation for species A in terms of the molar flux

$$\frac{\partial C_A}{\partial t} = -\left(\nabla \cdot \vec{N}_A\right) + \dot{R}_{A,G} \tag{4.}$$

Rectangular coordinates (x, y, z)

$$\frac{\partial C_A}{\partial t} = -\left(\frac{\partial [N_A]_z}{\partial x} + \frac{\partial [N_A]_y}{\partial y} + \frac{\partial [N_A]_z}{\partial z}\right) + \dot{R}_{A,G}$$
(4a)

Cylindrical coordinates (r,  $\theta$ , z)  $\frac{\partial C_A}{\partial t} = -\left\{\frac{1}{r}\frac{\partial}{\partial r}[rN_A]_r + \frac{1}{r}\frac{\partial}{\partial \theta}[N_A]_{\theta} + \frac{\partial}{\partial z}[N_A]_z\right\} + \dot{R}_{A,G}$ (4b)

Spherical coordinates  $(r, \theta, \phi)$ 

$$\frac{\partial C_A}{\partial t} = -\left\{\frac{1}{r^2}\frac{\partial}{\partial r}\left(r^2[N_A]_r\right) + \frac{1}{r\sin\theta}\frac{\partial}{\partial\theta}\left([N_A]_\theta\sin\theta\right) + \frac{1}{r\sin\theta}\frac{\partial}{\partial\phi}[N_A]_\phi\right\} + \dot{R}_{A,G}$$
(4c)

### 04-CHEM-B1, Transport Phenomena

May 2016

