

National Examinations December 2019

16-CHEM-A2, UNIT OPERATIONS and SEPARATION PROCESSES

3 hours duration

NOTES

1. If doubt exists as to the interpretation of any question, the candidate is urged to submit with the answer paper, a clear statement of any assumptions made.
2. The examination is an **open book exam**. One textbook of your choice with notations listed on the margins etc., but no loose notes are permitted into the exam.
3. Candidates may use any **non-communicating** scientific calculator.
4. All problems are worth 25 points. At least **two problems** from **each** of parts A and B must be attempted.
5. **Only the first two** questions as they appear in the answer book from each section will be marked.
6. State all assumptions clearly.

PART A: UNIT OPERATIONS

- A1. A liquid (density = 997.1 kg/m³, viscosity = 2.1×10^{-3} Pa.s) is pumped at 27 °C from an open tank through a 1-inch nominal diameter smooth sanitary pipe (inside diameter = 2.291 cm) to a second tank at a higher level. The mass flow rate is 1 kg/s through 30 m of straight pipe with two 90° standard elbows and one angle valve (fully open). The supply tank maintains a liquid level of 3 m, and the liquid leaves the system at elevation of 12 m above the floor. Compute the power requirements of the pump assuming an efficiency of 60%.
- A2. Spherical glass particles (12 mm diameter and 2500 kg/m³ density) and spherical metal particles (1.5 mm diameter and 7500 kg/m³) are falling in water (density = 1000 kg/m³).
- (a) [12.5 points] Calculate the terminal falling velocities of glass and metal particles in water for a constant friction factor of 0.22.
- (b) [12.5 points] At what water velocity will fluidized beds of glass particles and metal particles have the same bed densities? The relation between fluidization velocity (u_c), terminal velocity (u_0) and bed voidage (e) for a spherical particle is given by the equation $(u_c/u_0) = e^{2.3}$

- A3. A single-frame laboratory plate and frame filter press is used to filter water containing 1.39% mole fraction of calcium carbonate (CaCO_3). The density of solid calcium carbonate is 2830 kg/m^3 . Tests at a temperature of 19 °C and $\Delta P = 2.72 \text{ atm}$ gave the following results:

| Filtrate Volume (in liters) | Time (in seconds) |
|-----------------------------|-------------------|
| 0.2 | 1.8 |
| 0.4 | 4.2 |
| 0.6 | 7.5 |
| 0.8 | 11.2 |
| 1.0 | 15.4 |
| 1.2 | 20.5 |
| 1.4 | 26.7 |
| 1.6 | 33.4 |
| 1.8 | 41.0 |
| 2.0 | 48.8 |
| 2.2 | 57.7 |
| 2.4 | 67.2 |
| 2.6 | 77.3 |
| 2.8 | 88.7 |

The unit was 30 mm thick and had a filtering area of 263 cm^2 . Density of the dried cake was 1603 kg/m^3 . Determine the following:

- a) [12 points] Filtrate volume equivalent in resistance to the filter medium and piping
- b) [9 points] Specific cake resistance and cake porosity
- c) [4 points] Specific surface area of the cake

PART B: SEPARATION PROCESSES

- B1. A countercurrent rotary drier at 22 °C is fed granular material containing 40% moisture and the material is withdrawn at 32 °C containing 5% moisture. The air supplied, which contains 0.006 kg water vapor per kg of dry air, enters the drier at 112 °C and leaves at 37 °C. The drier handles 0.125 kg/sec wet stock of granular material. Assuming that radiation losses amount to 20,000 J/kg of dry air used, determine the following:
- (a) [18 points] Mass flow of dry air supplied to the drier
- (b) [7 points] Humidity of air leaving the drier.

DATA:

Specific heat capacity of dried granular material = 880 J/kg K
Specific heat capacity of dry air = 1000 J/kg K
Specific heat capacity of water vapor = 2010 J/kg K
Latent heat of water vapor at 22 °C = 2.449 MJ/kg

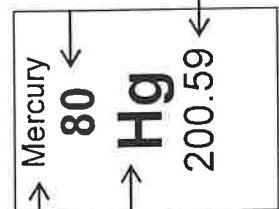
- B2. A salt ($\text{Na}_2\text{SO}_4 \cdot 10\text{H}_2\text{O}$) is to be produced in a Swenson-Walker crystallizer by cooling to 17 °C a solution of anhydrous Na_2SO_4 that saturates between 17 °C and 27 °C. The solubilities of anhydrous Na_2SO_4 in water are 40 kg/100 kg of water at 27 °C and 14 kg/100 kg water at 17 °C. The mean heat capacity of the liquor is 3.8 kJ/kg K and the heat of crystallization is 230 kJ/kg. For the crystallizer running in countercurrent flow mode, the available heat transfer area is 3 m^2/m length, the overall heat transfer coefficient is 0.15 kW/ $\text{m}^2 \text{K}$. If the cooling water enters the crystallizer at 7 °C and leaves at 17 °C with negligible evaporation, how many sections of the crystallizer will be required to process 0.25 kg/s of the product? Assume each section to be 3 m long.

- B3. A double-effect forward-feed evaporator is required to give a product, which contains 50% by mass of solids. Each effect has 10 m^2 of heating surface, and the heat transfer coefficient in the first effect is $2.8 \text{ kW/m}^2 \text{ K}$ and $1.7 \text{ kW/m}^2 \text{ K}$ in the second effect. Dry and saturated steam is available at a pressure of 375 kPa and the condenser operates at a pressure of 13.5 kPa. The concentrated solution exhibits a boiling-point rise of 3 K. What is the maximum permissible feed rate if feed contains 10% solids at 310 K? The latent heat is 2330 kJ/kg and the specific heat capacity is 4.1868 kJ/kg under all the above conditions.

The Periodic Table of the Elements

1

| | | |
|--|---|---|
| Hydrogen 1 H 1.01 | Alkali metals 2 Li 6.94 | Alkaline earth metals 3 Ba 137.33 |
| Transition metals 4 Ti 47.88 | Transition metals 5 V 50.94 | Transition metals 6 Cr 52.00 |
| Other metals 6 Nb 92.91 | Manganese 7 Mn 54.94 | Chromium 8 Cr 52.00 |
| Metalloids (semi-metal) 7 Zr 91.22 | Titanium 8 Tc (98) | Iron 9 Fe 56.94 |
| Nonmetals 8 Y 88.91 | Nickel 9 Ni 58.69 | Cobalt 10 Co 58.93 |
| Halogens 10 Cl 35.45 | Iron 11 Fe 56.94 | Manganese 12 Mn 54.94 |
| Noble gases 11 Na 22.99 | Scandium 13 Sc 44.96 | Scandium 14 Sc 44.96 |
| 12 Mg 24.31 | Titanium 15 Ti 47.88 | Titanium 16 Ti 47.88 |



| Element name → | Atomic # ← | Symbol | Avg. Mass |
|----------------|------------|-----------|-----------|
| Mercury | 80 | Hg | 200.59 |
| Scandium | 21 | Sc | 44.96 |
| Titanium | 22 | Ti | 47.88 |
| Vanadium | 23 | V | 50.94 |
| Chromium | 24 | Cr | 52.00 |
| Manganese | 25 | Mn | 54.94 |
| Iron | 26 | Fe | 56.94 |
| Cobalt | 27 | Co | 58.93 |
| Nickel | 28 | Ni | 58.69 |
| Copper | 29 | Cu | 63.55 |
| Zinc | 30 | Zn | 65.39 |
| Gallium | 31 | Ga | 69.72 |
| Germanium | 32 | Ge | 72.61 |
| Arsenic | 33 | As | 74.92 |
| Selenium | 34 | Se | 78.96 |
| Bromine | 35 | Br | 79.90 |
| Fluorine | 9 | F | 19.00 |
| Oxygen | 8 | O | 16.00 |
| Nitrogen | 7 | N | 14.01 |
| Boron | 5 | B | 10.81 |
| Carbon | 6 | C | 12.01 |
| Aluminum | 13 | Al | 26.98 |
| Silicon | 14 | Si | 28.09 |
| Phosphorus | 15 | P | 30.97 |
| Sulfur | 16 | S | 32.07 |
| Chlorine | 17 | Cl | 36.45 |
| Argon | 18 | Ar | 39.95 |
| Neon | 10 | Ne | 20.18 |
| Helium | 2 | He | 4.00 |

| | | | | | | | | | | | | | | |
|--------------|--|---|---|---|---------------------------------------|---------------------------------------|--|--|--|---|---|--|--|------------------------------------|
| *lanthanides | Lanthanum 57 La 138.91 | Praseodymium 58 Ce 140.12 | Neodymium 59 Pr 140.91 | Promethium 61 Pm (145) | Samarium 62 Sm 150.36 | Europium 63 Eu 151.97 | Gadolinium 64 Gd 157.25 | Terbium 65 Tb 158.93 | Dysprosium 66 Dy 162.50 | Holmium 67 Ho 164.93 | Erbium 68 Er 167.26 | Thulium 69 Tm 168.93 | Ytterbium 70 Yb 173.04 | |
| Actinides | Actinium 89 Ac (227) | Thorium 90 Th 232.04 | Protactinium 91 Pa 231.04 | Uranium 92 U 238.03 | Neptunium 93 Np (237) | Plutonium 94 Pu (244) | Americium 95 Am (243) | Curium 96 Cm (247) | Berkelium 97 Bk (247) | Californium 98 Cf (251) | Fermium 99 Es (252) | Mendelevium 100 Fm (257) | Nobelium 102 No (259) | |
| ** actinides | Radium 88 Ra (226) | Lawrencium 103 Lr (262) | Dubnium 104 Rf (267) | Seaborgium 105 Ds (271) | Bohrium 106 Bh (272) | Hassium 108 Hs (270) | Mendelevium 109 Mt (276) | Roentgenium 110 Rg (280) | Copernicium 112 Cn (285) | Ununtrium 113 Uut (284) | Ununpentium 115 Uup (288) | Ununhexium 116 Uuh (293) | Ununseptium 117 Uus (294?) | Radium 86 Rn (222) |

TABLE B.2 Saturated Water: Pressure Table

| P kPa, MPa | T °C | \hat{v}_1 m^3/kg | \hat{v}_o m^3/kg | \hat{u}_1 kJ/kg | $\Delta\hat{u}_o$ kJ/kg | \hat{u}_o kJ/kg | f_1 kJ/kg | Δf_o kJ/kg | f_o kJ/kg | \hat{s}_1 kJ/kg K | $\Delta\hat{s}_o$ kJ/kg K | \hat{s}_o kJ/kg K |
|---------------|---------|-------------------------|-------------------------|----------------------|----------------------------|----------------------|----------------|-----------------------|----------------|------------------------|------------------------------|------------------------|
| 0.6113 | 0.01 | 0.001000 | 206.132 | 0 | 2376.3 | 2376.3 | 0.00 | 2501.3 | 2501.3 | 0 | 9.1562 | 9.1562 |
| 1.0 | 6.98 | 0.001000 | 129.208 | 29.29 | 2355.7 | 2355.0 | 29.29 | 2494.9 | 2514.2 | 0.1059 | 8.8697 | 8.9756 |
| 1.5 | 13.03 | 0.001001 | 87.980 | 54.70 | 2339.6 | 2339.3 | 54.70 | 2470.6 | 2525.3 | 0.1956 | 8.6322 | 8.8278 |
| 2.0 | 17.50 | 0.001001 | 67.004 | 73.47 | 2326.0 | 2309.5 | 73.47 | 2460.0 | 2533.5 | 0.2607 | 8.4629 | 8.7236 |
| 2.5 | 21.08 | 0.001002 | 54.254 | 88.47 | 2315.9 | 2404.4 | 88.47 | 2451.6 | 2540.0 | 0.3120 | 8.3111 | 8.6431 |
| 3.0 | 24.08 | 0.001003 | 45.665 | 101.03 | 2307.5 | 2408.5 | 101.03 | 2444.5 | 2545.5 | 0.3545 | 8.2231 | 8.5775 |
| 4.0 | 28.96 | 0.001004 | 34.800 | 121.44 | 2293.7 | 2415.2 | 121.44 | 2422.9 | 2554.4 | 0.4226 | 8.0520 | 8.4746 |
| 5.0 | 32.88 | 0.001005 | 28.193 | 137.79 | 2282.7 | 2420.5 | 137.79 | 2423.7 | 2561.4 | 0.4763 | 7.9187 | 8.3950 |
| 7.5 | 40.29 | 0.001008 | 19.238 | 168.76 | 2261.7 | 2430.5 | 168.77 | 2406.0 | 2574.8 | 0.5763 | 7.6751 | 8.2514 |
| 10.0 | 45.81 | 0.001010 | 14.674 | 191.79 | 2246.1 | 2437.9 | 191.81 | 2392.8 | 2584.6 | 0.6492 | 7.5010 | 8.1501 |
| 15.0 | 53.97 | 0.001014 | 10.022 | 225.90 | 2232.8 | 2448.7 | 225.91 | 2373.1 | 2599.1 | 0.7548 | 7.2595 | 8.0084 |
| 20.0 | 60.06 | 0.001017 | 7.649 | 251.35 | 2205.4 | 2456.7 | 251.38 | 2359.3 | 2609.7 | 0.8219 | 7.0766 | 7.9085 |
| 25.0 | 64.97 | 0.001020 | 6.204 | 271.89 | 2191.2 | 2463.1 | 271.90 | 2946.3 | 2618.2 | 0.8930 | 6.9383 | 7.8313 |
| 30.0 | 69.10 | 0.001022 | 5.229 | 289.18 | 2179.2 | 2468.4 | 289.21 | 2326.1 | 2625.3 | 0.9439 | 6.8247 | 7.7685 |
| 40.0 | 75.87 | 0.001026 | 3.993 | 317.51 | 2158.5 | 2477.0 | 317.55 | 2319.2 | 2636.7 | 1.0258 | 6.6441 | 7.6700 |
| 50.0 | 81.33 | 0.001030 | 3.240 | 340.42 | 2143.4 | 2483.8 | 340.47 | 2305.4 | 3645.9 | 1.0910 | 6.5029 | 7.5829 |
| 75.0 | 91.77 | 0.001037 | 2.217 | 384.29 | 2112.4 | 2496.7 | 384.36 | 3278.6 | 3663.0 | 1.2125 | 6.2434 | 7.4563 |
| 0.100 | 92.62 | 0.001043 | 1.6940 | 417.33 | 2088.7 | 2506.1 | 417.44 | 2258.0 | 2675.5 | 1.3025 | 6.0568 | 7.3593 |
| 0.125 | 105.99 | 0.001048 | 1.3749 | 444.16 | 2069.3 | 2513.5 | 444.30 | 2241.1 | 2685.3 | 1.3739 | 5.9104 | 7.2843 |
| 0.150 | 111.37 | 0.001053 | 1.1593 | 466.92 | 2052.7 | 2519.6 | 467.03 | 2226.5 | 2693.5 | 1.4235 | 5.7897 | 7.2232 |
| 0.175 | 116.06 | 0.001057 | 1.0036 | 486.78 | 2038.1 | 2524.9 | 486.97 | 2213.6 | 2700.5 | 1.4848 | 5.6868 | 7.1717 |
| 0.200 | 120.23 | 0.001061 | 0.8857 | 504.47 | 2025.0 | 2529.5 | 504.68 | 2202.0 | 2706.6 | 1.5300 | 5.5970 | 7.1271 |
| 0.225 | 124.00 | 0.001064 | 0.7933 | 520.45 | 2013.1 | 2533.6 | 520.69 | 2191.3 | 2712.0 | 1.5705 | 5.5173 | 7.0578 |
| 0.250 | 127.43 | 0.001057 | 0.7187 | 535.08 | 2002.1 | 2537.2 | 535.34 | 2181.5 | 2716.9 | 1.6072 | 5.4455 | 7.0526 |
| 0.275 | 130.60 | 0.001070 | 0.6573 | 548.57 | 1992.0 | 2540.5 | 548.87 | 2172.4 | 2721.3 | 1.6407 | 5.3801 | 7.0208 |
| 0.300 | 133.55 | 0.001073 | 0.6058 | 561.13 | 1982.4 | 2543.6 | 561.45 | 2163.9 | 2725.3 | 1.6717 | 5.3201 | 6.9918 |
| 0.325 | 136.30 | 0.001076 | 0.5620 | 572.88 | 1973.6 | 2546.3 | 573.23 | 2155.8 | 2729.0 | 1.7005 | 5.2646 | 6.9651 |
| 0.350 | 138.88 | 0.001079 | 0.5243 | 583.93 | 1965.0 | 2548.9 | 584.31 | 2148.1 | 2732.4 | 1.7274 | 5.2130 | 6.9404 |
| 0.375 | 141.32 | 0.001081 | 0.4914 | 594.38 | 1956.9 | 2551.3 | 594.79 | 2140.8 | 2735.6 | 1.7527 | 5.1647 | 6.9174 |
| 0.40 | 143.63 | 0.001084 | 0.4625 | 604.29 | 1949.2 | 2553.6 | 604.73 | 2133.8 | 2738.5 | 1.7766 | 5.1193 | 6.8958 |
| 0.45 | 147.93 | 0.001088 | 0.4140 | 622.75 | 1934.9 | 2557.6 | 623.24 | 2120.7 | 2743.9 | 1.8206 | 5.0359 | 6.8565 |
| 0.50 | 151.86 | 0.001093 | 0.3749 | 639.66 | 1921.6 | 2561.2 | 640.21 | 2108.5 | 2748.7 | 1.8506 | 4.9806 | 6.8212 |
| 0.55 | 155.48 | 0.001097 | 0.3427 | 655.30 | 1909.2 | 2564.6 | 655.91 | 2087.0 | 2752.9 | 1.8972 | 4.8920 | 6.7892 |
| 0.60 | 158.85 | 0.001101 | 0.3157 | 669.88 | 1897.5 | 2567.4 | 670.54 | 2086.3 | 2756.8 | 1.9311 | 4.8269 | 6.7600 |
| 0.65 | 162.01 | 0.001104 | 0.2927 | 683.55 | 1886.5 | 2570.1 | 684.26 | 2076.0 | 2760.3 | 1.9627 | 4.7704 | 6.7320 |
| 0.70 | 164.97 | 0.001108 | 0.2729 | 696.43 | 1876.1 | 2572.6 | 697.20 | 2066.3 | 2763.5 | 1.9922 | 4.7158 | 6.7080 |