# 16-CHEM-A3, HEAT and MASS TRANSFER

#### **DECEMBER 2019**

### **Three Hours Duration**

### **NOTES:**

- 1) If doubt exists as to the interpretation of any question, you are urged to submit a clear statement of any assumptions made along with the answer paper.
- 2) Property data required to solve a given problem are provided in the problem statement or are available in the recommended texts. If you are unable to locate the required data, do not let this prevent you from solving the rest of the problem. Even in the absence of property data, you still have the opportunity to provide a solution methodology.
- 3) This is an **open-book exam**. One textbook of your choice with notations listed on the margins etc., but no loose notes are permitted into the exam. Candidates may use any **non-communicating** calculator.
- 4) All problems are worth 25 points. At least two problems from each part must be attempted.
- 5) Only the first two questions as they appear in the answer book from each section will be marked.

# PART A - HEAT TRANSFER

1) A solution containing 500 kg of Na<sub>2</sub>SO<sub>4</sub> in 2500 kg of water is cooled from 50 °C to 10 °C in an agitated mild steel vessel of mass 750 kg. At 10 °C, the solubility of the anhydrous salt is 8.9 kg per 100 kg of water and the stable crystalline phase is Na<sub>2</sub>SO<sub>4</sub>.10H<sub>2</sub>O. If 2% of the water initially present is lost by evaporation during cooling, estimate the heat that must be removed.

DATA: Heat of solution at  $18 \, ^{\circ}\text{C} = -78.5 \, \text{kJ/mol}$ 

Specific heat capacity of Na<sub>2</sub>SO<sub>4</sub> solution = 3.6 kJ/kg K

Specific heat capacity of mild steel = 0.5 kJ/kg K

2) A vertical plate (15 cm x 15 cm) at 40 °C is exposed to ambient still air at 20 °C. Compare the free convection heat transfer rate from the plate to the forced convection heat transfer rate that would result at a velocity equal to twice the maximum velocity under free convection conditions. The thermo-physical properties of dry air at atmospheric pressure are given below:

$\overline{T}$	ρ	μ	κ	$C_p$	$\rho/\mu$	$g\beta/(\nu\alpha)$	$\alpha$
[K]	$\left[\frac{kg}{m^3}\right]$	$\left[10^{-6} \frac{N \cdot s}{m^2}\right]$	$\left[10^{-3} \frac{W}{m \cdot K}\right]$	$\left[\frac{J}{kg\cdot K}\right]$	$\left[10^3 \frac{s}{m^2}\right]$	$\left[10^6 \frac{1}{m^3 \cdot K}\right]$	$\left[10^{-6}\frac{m^2}{s}\right]$
200	1.7690	13.36	18.10	1006.4	132.4	638.6	10.17
210	1.6842	13.92	18.95	1006.1	121.0	505.2	11.18
220	1.6071	14.47	19.80	1005.7	111.1	404.2	12.25
230	1.5368	15.01	20.63	1005.6	102.4	327.0	13.35
240	1.4728	15.54	21.45	1005.5	94.8	267.3	14.49
250	1.4133	16.06	22.26	1005.4	88.0	220.4	15.67
260	1.3587	16.57	23.05	1005.5	82.0	183.3	16.87
270	1.3082	17.07	23.84	1005.5	76.6	153.6	18.12
280	1.2614	17.57	24.61	1005.7	71.8	129.6	19.40
290	1.2177	18.05	25.38	1006.0	67.5	110.1	20.72
300	1.1769	18.53	26.14	1006.3	63.5	94.1	22.07
310	1.1389	19.00	26.87	1006.8	59.9	80.9	23.43
320	1.1032	19.46	27.59	1007.3	56.7	70.0	24.83
330	1.0697	19.92	28.30	1007.9	53.7	60.8	26.25
340	1.0382	20.37	29.00	1008.5	51.0	53.1	27.70
350	1.0086	20.81	29.70	1009.2	48.5	46.5	29.18
360	0.9805	21.25	30.39	1010.0	46.1	41.0	30.69
370	0.9539	21.68	31.07	1010.9	44.0	36.2	32.22
380	0.9288	22.11	31.73	1012.0	42.0	32.1	33.76
390	0.9050	22.52	32.39	1013.0	40.2	28.6	35.33
400	0.8822	22.94	33.05	1014.2	38.5	25.5	36.94

3) A shell-and-tube heat exchanger consists of 120 tubes of 22-mm internal diameter and length of 2.5 m. It is operated as a single-pass condenser with benzene condensing at a temperature of 350 K on the outside of the tubes and water at inlet temperature of 290 K passing through the tubes. Initially there is no scale on the walls, and a rate of condensation of 4 kg/s is obtained with a water velocity of 70 cm/s through the tubes. After prolonged operation, a scale resistance of 2 x 10<sup>-4</sup> m<sup>2</sup> K/W is formed on the inner surface of the tubes. Assuming the heat transfer coefficient on the water side is proportional to 0.8 power of velocity and the heat transfer coefficient for condensing vapor is 2.25 kW/m<sup>2</sup> K based on the inside area, to what value must the water velocity be changed in order to maintain the same rate of condensation? The latent heat of vaporization of benzene is 400 kJ/kg.

DATA:

Specific heat capacity of feed = 3.98 kJ/kg.K Latent heat of condensing steam at 202.65 kPa = 2202 kJ/kg

Latent heat of vaporization of water 333 K = 2383 kJ/kg

### PART B – MASS TRANSFER

1) A 4 cm³ mixture formed by adding 2 cm³ of acetone (CH₃-CO-CH₃) to 2 cm³ dibutyl phthalate (CO₂C₄Hҙ-C₀H₄-CO₂C₄Hҙ) is contained in a 6 mm diameter vertical glass tube immersed in a thermostat maintained at 42 °C. A stream of air at 42 °C and 101.325 kPa pressure is passed over the open top of the tube to maintain a zero-partial pressure of acetone vapor at that point. The liquid level is initially 11.5 mm below the top of the tube and the acetone vapor is transferred to the air stream by molecular diffusion alone. The dibutyl phthalate can be regarded as completely non-volatile and the partial pressure of acetone vapor may be calculated from Raoult's law on the assumption that the density of dibutyl phthalate is sufficiently greater than that of acetone for the liquid to be completely mixed.

Assuming the vapor is ideal and neglecting the effects of bulk flow in the vapor, calculate the time taken for the liquid level to fall to 5 cm below the top of the tube.

DATA: Vapor pressure of acetone at 42 °C = 60.5 kPaDiffusivity of acetone vapor in air at 42 °C =  $0.123 \text{ cm}^2/\text{s}$ Density of liquid acetone =  $764 \text{ kg/m}^3$ Density of liquid dibutyl phthalate =  $1048 \text{ kg/m}^3$ 

2) The heat transfer correlation for a liquid flowing over a single cylinder is given by the following equation for Nusselt number (Nu):

$$Nu = h D/k = (0.506 Re^{0.5} + 0.00141 Re) Pr^{0.33}$$

where  $h \rightarrow$  heat-transfer coefficient  $D \rightarrow$  diameter of cylinder

 $k \rightarrow$  thermal conductivity of cylinder Re  $\rightarrow$  Reynolds number = D v  $\rho/\mu$ 

 $Pr \rightarrow Prandtl \ number = C_p \mu/k$   $C_p \rightarrow specific \ heat \ capacity \ of \ liquid$ 

 $\mu \rightarrow \text{viscosity of liquid}$   $\rho \rightarrow \text{density of liquid}$ 

v → velocity of liquid

The above equation, in association with the Chilton-Colburn analogy, can be used to predict the mass-transfer coefficient for a cylinder.

Estimate the mass-transfer coefficient ( $k_L$ ) at 27 °C for the dissolution of sodium chloride from a cast cylinder (diameter = 1.5 cm) made of solid sodium chloride (NaCl) and placed perpendicular to a flowing stream of water at a velocity of 10 m/s.

<u>DATA</u>: Binary liquid diffusivity (D<sub>AB</sub>) at 18 °C =  $1.26 \times 10^{-5} \text{ cm}^2/\text{s}$ 

Viscosity of water at  $18 \, ^{\circ}\text{C} = 1.073 \, \text{x} \, 10^{-3} \, \text{Pa.s}$ 

Viscosity of water at 27 °C =  $8.76 \times 10^{-4}$  Pa.s

Density of water =  $996 \text{ kg/m}^3$ 

3) A mixture of benzene and toluene containing 44% mass of benzene is separated in a distillation column at 1 atm and reflux ratio of 4 to give a product of 96% mass benzene and a waste of 4% mass toluene. The equilibrium mole fraction data for benzene at 1 atm pressure is as follows:

Vapor Mole Fraction	Liquid Mole Fraction
0.21	0.1
0.37	0.2
0.51	0.3
0.64	0.4
0.72	0.5
0.79	0.6
0.86	0.7
0.91	0.8
0.96	0.9
0.98	0.95

- (a) Calculate the mole fraction on the second plate of the distillation column from the top.
- (b) Determine the number of plates required and the position of the feed if supplied to the column as liquid at its boiling point of 95 °C.
- (c) Find the minimum reflux ratio possible.
- (d) Find the minimum number of plates required.
- (e) If the feed is fed to the distillation column at 15 °C, find the number of plates required if the reflux ratio remains unchanged.

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Helium 2 4.00	Neon 10 <b>Ne</b> 20.18	Argon 18 <b>Ar</b> 39.95		Krypton 36	Ż {	83.80	Xenon 54	×e	131.29	Radon 86	R	(222)	Ununoctium 118	Ono	(294)
11	Fluorine 9 <b>F</b>	Chorine 17 CI 35.45		Bromine 35	ក់	79.90	lodine 53	-	126.90	Astatine 85	Αt	(210)	Ununseptium 117	Nus	(294?)
91	Oxygen 8	Sulfur 16 S 32.07		Selenium 34	Se	78.96	Tellurium 52	Te	127.60	Polonium 84	Ро	(509)	Ununhexium 116	Ouh	(293)
5	Nitrogen 7 N 14.01	Phosphorus 15 P 30.97		Arsenic 33	As	74.92	Antimony 51	Sp	121.76	Bismuth 83	ä	208.98	Ununpentium 115	Uup	(288)
4	Carbon 6 C 12.01	Silicon 14 Si.09		Germanlum 32	Ge	72.61	Tin 50	Sn	118.71	Lead 82	Pb	207.20	Ununquadium 114	Ouq	(289)
5	Boron 5	Auminum 13 A1 26.98		Sallium 31	Ga	69.72	Indium 49	드	114.82	Thellium 81	F	204.38	Ununtrium 113	Out	(284)
#	Avg. Mass	- In	12	30 30	Zu	65.39	Cadmium 48	ဦ	112.41	Mercury 80	Hg	200.59	Copernicium 112	ပ	(285)
Atomic #	– Avg.		1	Copper 29	D C	63.55	Silver 47	Ag	107.87	Gold 79	Au	196.97	Roenigenium 111	Rg	(280)
Sury • • • • • • • • • • • • • • • • • • •	<b>⊙</b>		10	Nickel 28	Z	58.69	Palladium 46	Pd	106.42	Platinum 78	ፈ	195.08	Darmstadfium 110	Ds	(281)
→ Mercury	200.59		6	Cobalt 27	ပိ	58.93	Rhodium 45	格	102.91	Iridium 77	<u>-</u>	192.22	Melinerium 109	Μţ	(276)
		<b></b>	8	Iron 26	Ьe	55.85	Ruthenium 44	Ru	101.07	Osmium 76	Os	190.23	Hassium 108	Hs	(270)
ment name.	် ဂ်		7	Manganese 25	Mn	54.94	Technetium 43	Δ	(86)	Rhenium 75	Re	186.21	Bohrium 107	Bh	(272)
Elem			9	Chromium 24	ပ်	52.00	Molybdenum 42	Ø	95.94	Tungsten 74	>	183.84	Seaborgium 106	Sg	(271)
netals Is			2	Vanadlum 23	>	50.94	Niobium 41	QN N	92.91	Tantalum 73	Та	180.95	Dubnium 105	Op	(268)
Alkali metals Alkaline earth metals Transition metals Other metals	Nonmetals Halogens Noble gases		4	Titanium 22	ï	47.88	Zirconium 40	Zr	91.22	Hathium 72	Ï	178.49	Rutherfordium 104	¥	(267)
Alka Alka Tran Othe	Non Nob Nob		က	Scandium 21	သွင	44.96	Ymium 39	>	88.91	Lutetium 71	Γn	174.97	Lawrencium 103	ב	(262)
										67.70	*		89.102	*	
2	Beryllum 4 Be 9.01	Magnesium 12 Mg 24.31		Calcium 20	Ca	40.08	Stronfium 38	ร	87.62	Barium 56	Ва	137.33	Radium 88	Ra	(226)
Hydrogen 1,01	Lithium 3 Li 6.94	11 Na 22.99		Potassium 19	ヱ	39.10	Rubidium 37	Sp.	85.47	Cesium 55	S	132.91	Francium 87	ř	(223)

	Lanthanum 57	Cerium 558	Praseodymium 59	Neodymішт 60	Promethium 61	Samanum 62	Europium 63	Gadolinium 64	Terbium 65	Dysprosium 66	Holmium 67	Erbium 68	Thullum 69	Ytterbium 70
*lanthanides	Ľ	င် င	P	PZ	Pm	Sm	En	gg	유	ò	운	ம்	Tm	Υb
	138.91	140.12	140.91	144.24	(145)	150.36	151.97	157.25	158.93	162.50	164.93	167.26	168.93	173.04
	Actinium	Thorium	Protactinium	Uranium	Neptunium	Plutonium	Americium	Curium	Berkelium	Californium	Einsteinium	Fermium	Mendelevium	Nobelium
	83	90	91	92	93	94	92	96	97	86	66	100	101	102
**actinides	Ac	느	Ра	_	Q N	Pu	Am	S	益	ຽ	Es	Fm	Md	å
	(227)	232.04	231.04	238.03	(237)	(244)	(243)	(247)	(247)	(251)	(252)	(257)	(258)	(52)

